Notebook, N-Undated.2

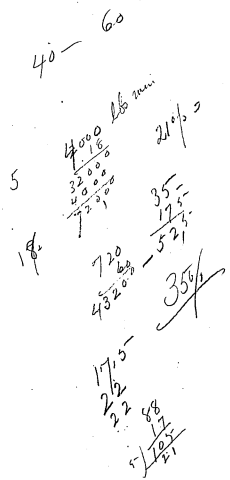
This undated notebook was probably used sometime during the period 1901-1902. All entries are by Edison. The book contains notes and drawings regarding the technical details of cement production. Included are items pertaining to the temperature of the kiln in the roasting process and the degree of fineness needed in the ground cement rock. The pages are unnumbered. Approximately 170 pages have been used.

N-00-00-00.2

Burning Portland Cement -

It is stated by Expert of Lehigh Cement Co that they use 150 lbs of powdered bituminous Coal per bbl of Portland Cement presumably 400 lbs -
That the terminal temperature of gases leaving roasters is 1600 deg Fahr. If this is Correct. The Heat units with 7% ash 140 lbs Carbon would be

BTU 16,240,000



HU in Exit gases 540 deg above the temp of atmosphere 60 Fahr is

2.467.000

Expulsion of CO_2 from CaO-

1.940.000

Radiation assumed as 350 or 290 above the atmosphere from furnace & Cylinder

1.074 000

HU in Clinker supposing it leaves burner at 2000 Fahr

1.364.000

Decomposition of 19 lbs of water in air of combustion

133,000

Dehydration of silica -

125 000 -

Heat of clinkering or semifusion - 1,500,000

HU in fuel	16 240 000
	2 467 000
Exit gases	1 940 000
Explan CO_2	1 074 000
Radiation	1 364 000
in Clinker	1 600 000
Clinkering	133 000
Water	125 000
Dehydrat	8703 000

16 240 000
8 703 000
Unaccounted for- 7,537,000

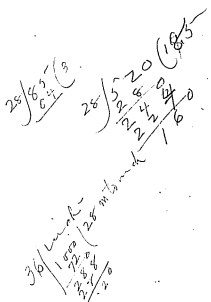
Either the Exit gases have a much higher temperature than stated or the temp of Cylinder is much higher than 350° or the Coal is not burnt to CO_2 but to CO or there is a great excess of air which would give more Exit gases —

The analyses show that the temp of exit gases must be low, that the C must be burnt to CO_2 with some excess of air to diminish vapor tension of CO_2 to permit Expulsion at low temp from Limestone —
That Regenerative device must be used on Clinker -

The Speed of the gases through 6 ft cylinder is 122 ft per minute which should not blow out

fine grinding of the Limestone & Cement rock. A thorough mixing is very important before going to roaster – as well as proportioning the rock to give no free Lime to clog the fire brick or hurt the Cement.

Note – Decompn of $CaCO_3$ starts at 440 C = 824 Fahr
If the pressure is kept below the limiting pressure or maximum Vapor tension the whole of the $CaCO_3$ is decomposed



Vapor pressure of CO_2 from $CaCO_3$
at 860 C or 1580 Fahr
is 85 mm (3 inches) of Mercury
at 1040 C or 1870 Fahr it
is 520 mm (18 inches) of Mercury

Caustic Lime Combines with
incandescence with CO_2
at 550 C or 1022 Fahr
The Compound formed is
$(CaO)_2\,CO_2$ The Compound is
capable of absorbing more CO_2

23.8

2 | 75
37.5
3
112.1

23.8
17.8
6.0

23.8
3
17.4

4 | 17.80
4.4.5
13.35

77.8
67
1246
1068
10 | 11.923
59630

23.8
2.5
19.0
476.0
59.5

17.8
5
89.0

67 ton Crushing 6 cheaves
75 lbs — 17.8 %

with 9 cheaves in 50 lbs to
the same thing =
hence 67 ton 17.8 gwes
gwes 59.6 66 lbs
100 tons with 17.8 gwes 89 66/100 —

112 lbs pressure gwes 23.8
75 — 17.8
6 difference

50% more pressure gives
only 25% more fines —
hence Reduction of 37.5 lbs.
pressure should reduce it
Certainly not less than 25%
or to 13.35 — The power
would be reduced from 75 to 37.5 —

hence 128 tons would go through on 35 lbs pressure gives 17.08 tons —

12 | 80 | 6,6
72
8 0

14
66
84
84
92 2

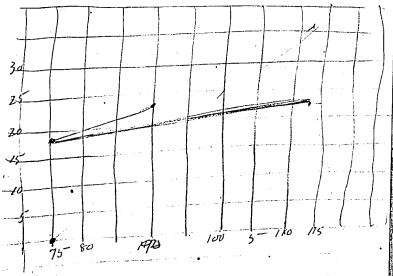
15
66
90
90
90 0

15 4/4"

1333
124
1068 0
1067
2
13335 80
17008

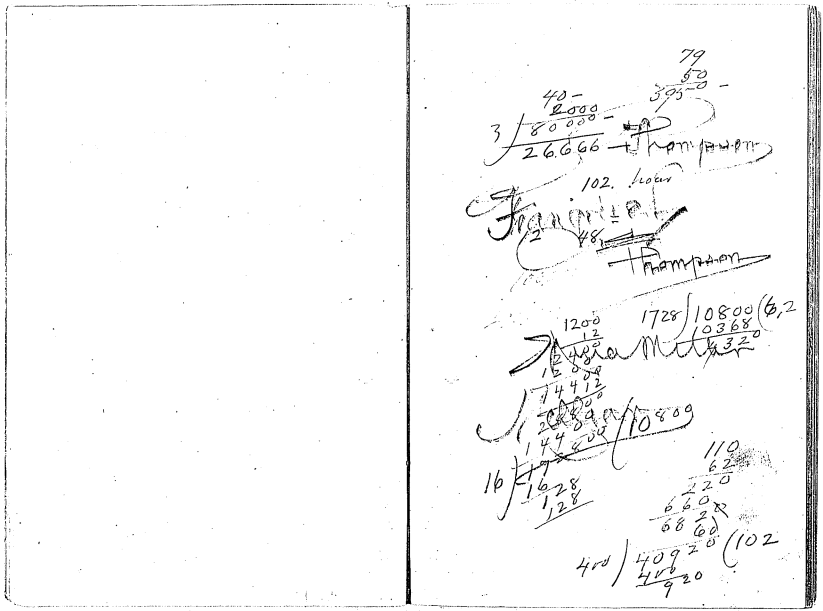
80 66 2/3

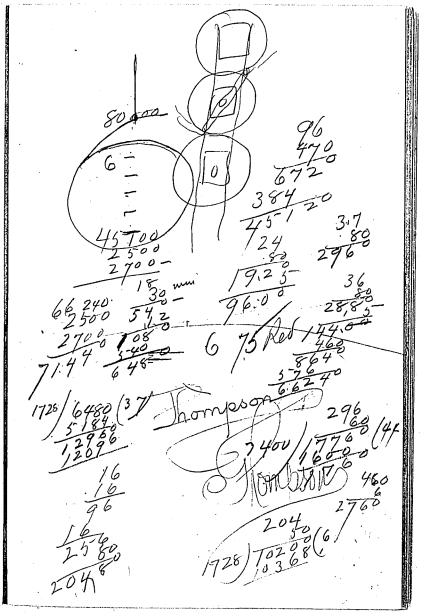
100
25

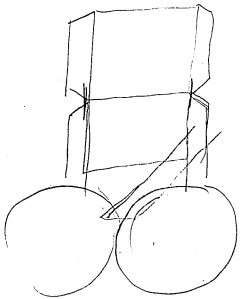


20% on 800 tons
16 2/3% on 1000 tons —
1/4 flake —

125
16
750
125
2000




Thompson



25
900
22-5 00
1

9720
25
48600
19440
500
8 | 2418
3037

1728 | 182220 | 105
1728
9440
8640

2240
1250
1120
1248
2240
2800

2.256 | 29296

105
130
315
105
13650

3037.00
1822 2

90
678
12
620
610
97
20

16 100
7/8 - 200
1/4 - 400
1/2 800 - 600

9720
96 | 291600 - (3037
288
360
3456
72

48 | 1200 (25
96
240
240

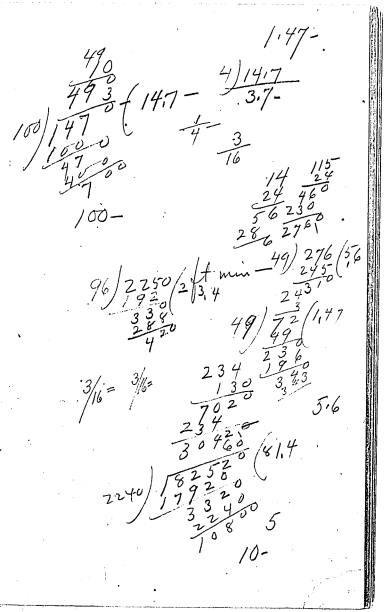
2500
60
4 | 150000 (375
120000
12000
3000
2500
2000

1728 | 3037 (1.7
1728
13096
12096

130
17
910
130
2211

170

230
13800



3555
35
17775
10665
2
12442
6221
47 40
79
25370
3318-00
5555
448
6
505-6
34-8
471 79
40
37.6

62000.16

pressure of
1 on 1
Mass 003 -
3 mass 09
hence 3 times work
atmospheric pressure

20
30
600 -

3555

474
35
237
1422
16590

1659.
35
82952
3580 65
29032

4977 lbs every 2 minutes

39

28.
3
84 - tons -

4) 25-00
6,25
1875 - 2

50
15
400
28
35
40
84
98

35 2000 ft 116 mi - 25
60 70 00 4
6000
1000
1600
4

116
4
696
2240 2776 (18.
2240
536
1936

Air motor
Rehearsal - Drill -
Ontz
Coal separation
Fine coal burning
Meters
Storage Cell
Marconi
Portland Cement

500 Hp

363
726

1200 100000
2400000 | 363
99000 | 125
21900 | 488
1200

850 Hp

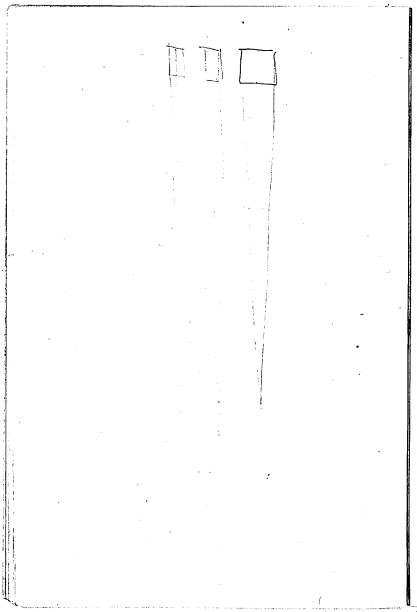
600 -

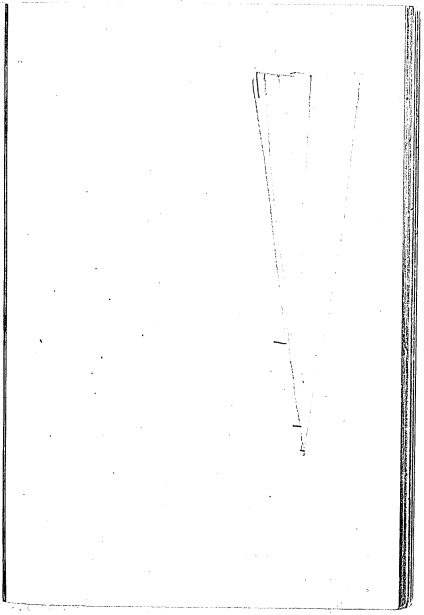
1/1200 - | 100000

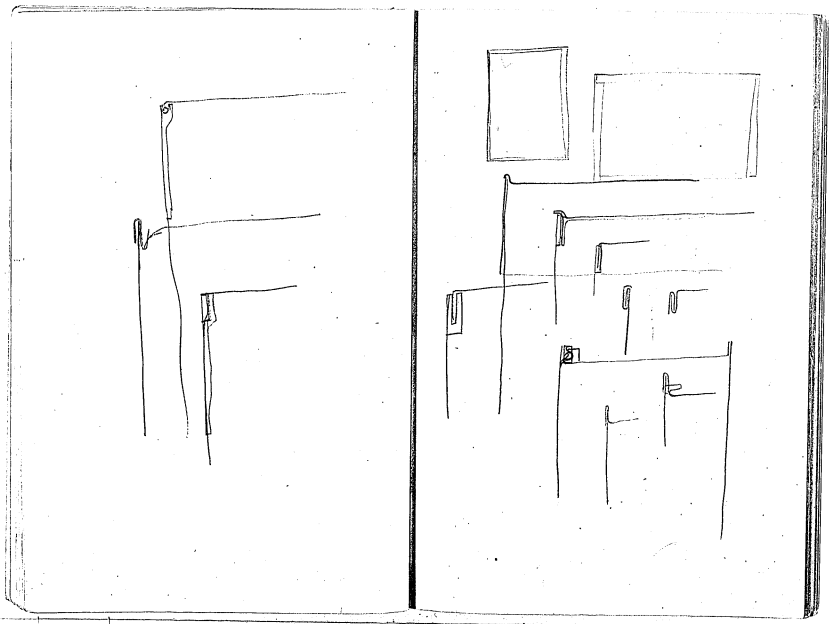
1200000

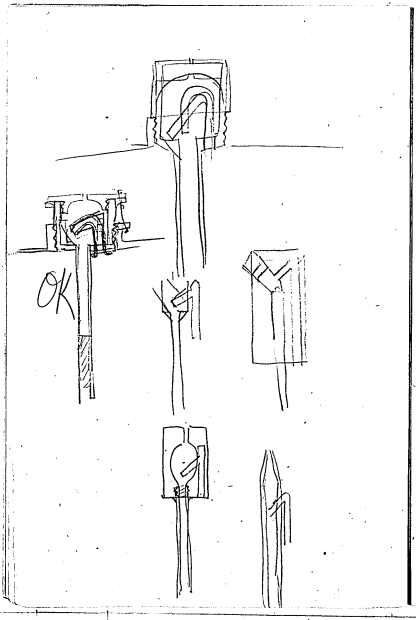
144
288

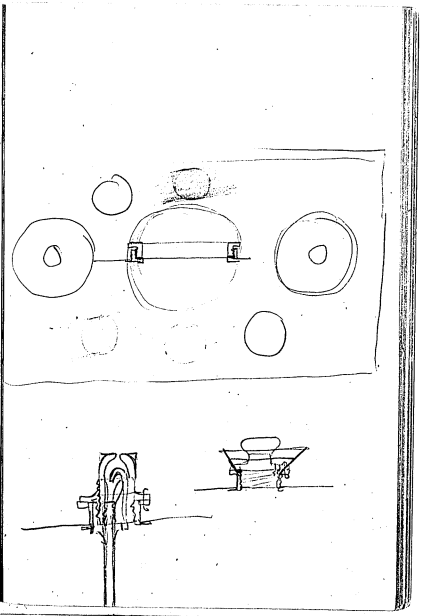
288 / 100000 (347
864
1360
1152
208

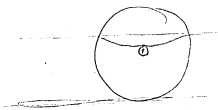







OK





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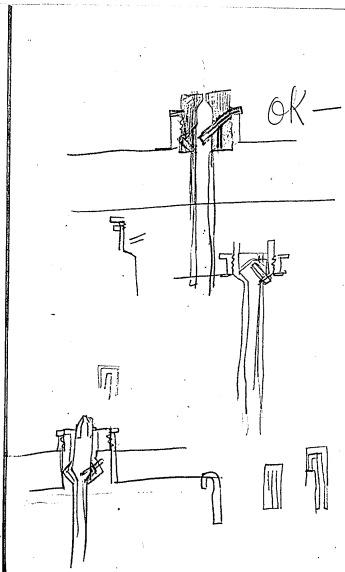

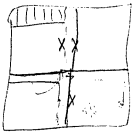

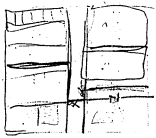

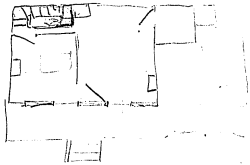

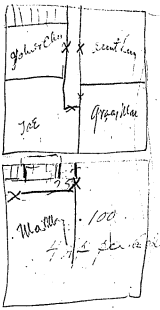

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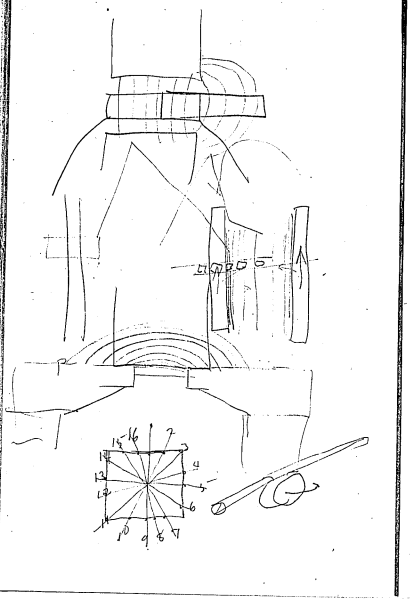
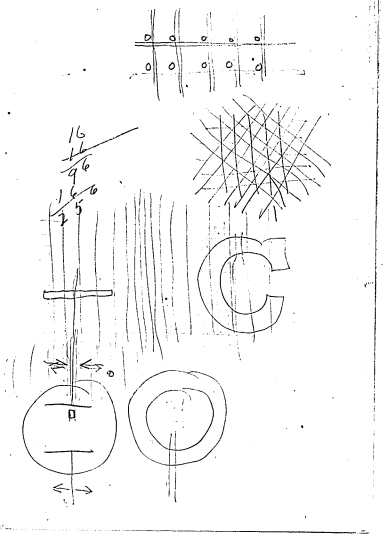
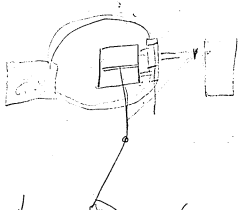






8384 / 8380000 (99
75-
83
24
00

99 miles

Zinc 55 lbs – 15¢ 825
55 20 1150
559400 / 925
75
20-
55 / 279700
20
1100 / 39 / 58 00 00 / 14-
4195-5-0-0
53-
7 5-
75
82 / 419000 net

55 / 444
300
1400 / 1332 00 60
15
799 20 67
55 / 5594 / 1263
55
8
40
825-
265

1 cell 419000 net ft. lbs –
20 cells –
8,380,000

55 / 40 / 80
20
8 / 1600 – 5240
16
200 – 3144 0
5240
8384 0

36 / 2000 / 55
180
200

HCl – fused NaCl, H_2SO_4

NH_4 — H_2SO_4

$CaCO_3$ —— Caustic K

CaO,CO_2. Pour Mercury & H_2SO_4 giving CO_2 mixed with O– Thence through a heater to Expansion Cylinder

If there was 32% fines in the 67. Tin + all the 009 came through with it There would be 34% on 200 mesh – but not more than ½ will come through while ¾ of float come through hence 27.8 on 200 mesh

lb
34
66 float

hence –

17
44
61

28
180
224

3/66
22

12

420

120

79
120
54
54
0

1.5
54
6
75
8.1

5.4

1990 000

Total in 61. 009
" " 13
74

3.6% float in — 82.5 009
17.5 float —
17.1 of 009 —

Had there been
7.2% of float
70 009
80 - float

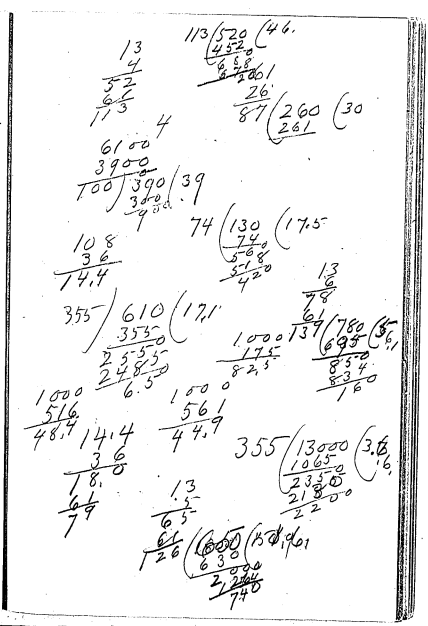
10.8 float. 61 009
39 float

with 14.4 float
54 000
46 float

25.2% 40.000
60 37
63 1200
252 180 float —
28 24
66
32% float 21.6 float

48.4
51.6

44.9
56.1



82.5 009
17.5 flour —

70 - 009
30 flour —

30.5
130
43 / 1300 (30
1305

12
104
6
165 (1040 (10
990
50
15

61
26 -
87 (260 (30
261

36
8
288

13
8
104
6
165 (1040 (

115 -
70
45

3
29
5
260
228
32

45%

15
18
30
15 0
27
3 4 7 3
8
27
13

36
9
324

82.5 009
17.5 flour 13 - 61

1000
173
25

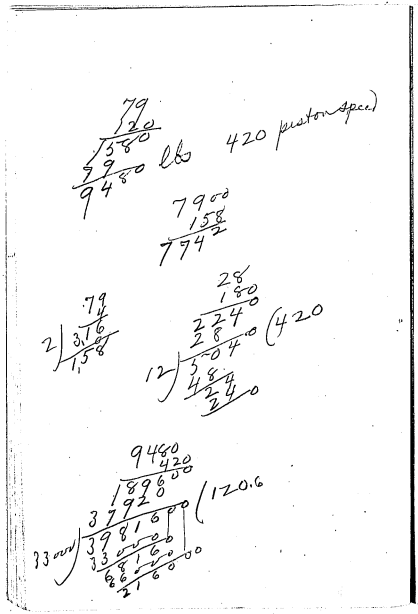
13
74 (130 (1
74
56
8
4

90 - flour - flavor - 20% used 90 days
10% flour —
101 lbs + sauce like 10% —
202 lbs — flour 10% —
91 20% — flour 90 —
where left 70 lbs 20% corn —
91 20% flour on 200 —
Where — 25% 1 20% corn —

$$\begin{array}{r} 36 \\ 7 \\ \hline 252 \end{array}$$

$$\begin{array}{r} 13 \\ 7 \\ \hline 91 \end{array}$$

$$\begin{array}{r} 61 \\ 52 \\ \hline 9 \end{array} \overline{)9100} \overline{)60}$$



70
35
35-0
210
243-0

60
48
2880-

70 —

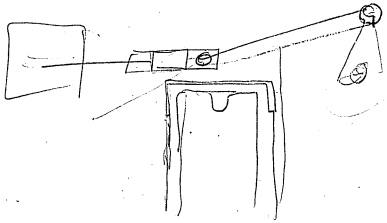
355
26
2130
710
9230

92 grms

32
6400
26
384
1281
1601
1600

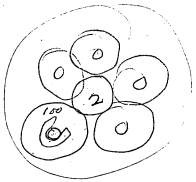
400 | 40 66 Rs

12 | 90000 | 7500
84
60
60



1000

200 Rev min
1000 lbs cut
$\frac{1}{20}$ of cut friction
6" bar Rev 200 Rev.
100 ft per min



5000 ft lbs
625 11

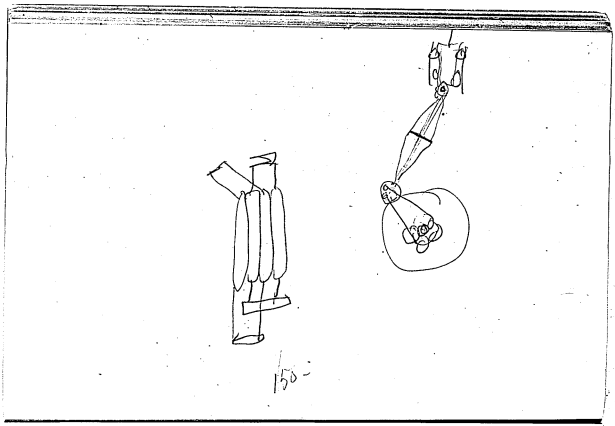
12.5 ft min

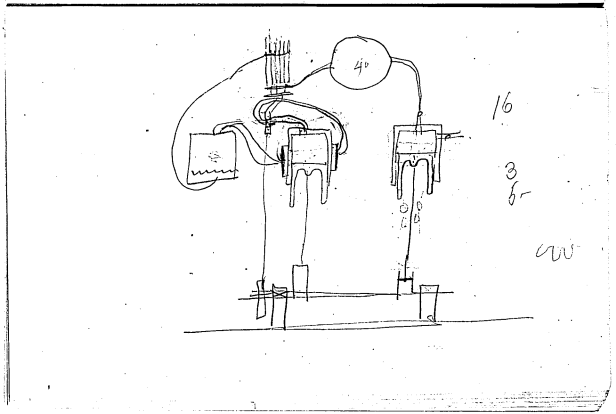
$12\overline{)150}$ $\frac{12.5}{20}$
$\frac{3}{20}$
$\frac{20}{60}$

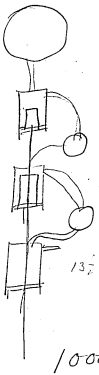
$62\overline{)5000}$ $\frac{50}{20}$
$\frac{62.5}{}$

$\frac{62.5}{5000}$ $\frac{5000}{}$

Good
Good
Good

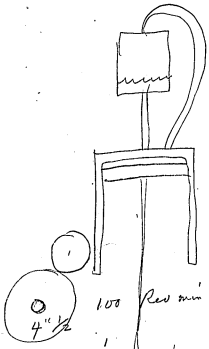

150-


40
16
3
6-



2"

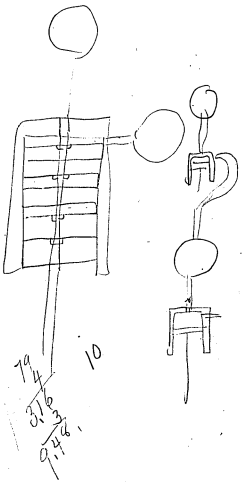
2" 100 ft min =
50 drag
5000 ft lbs



100
5000

50
300

16-times less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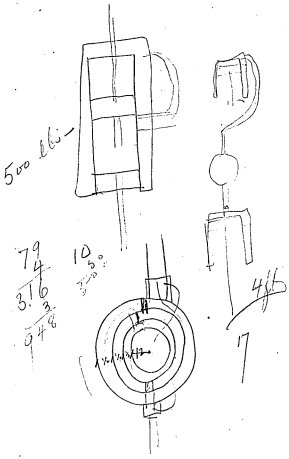
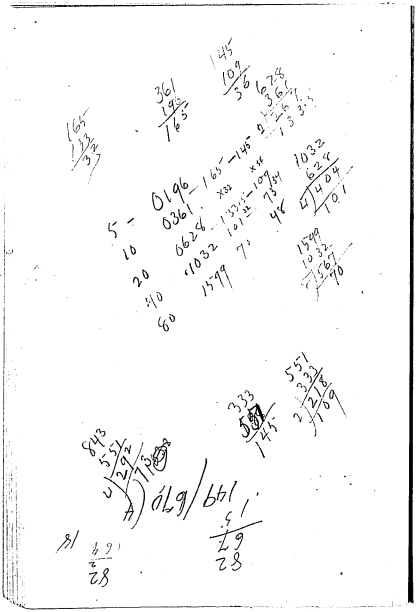
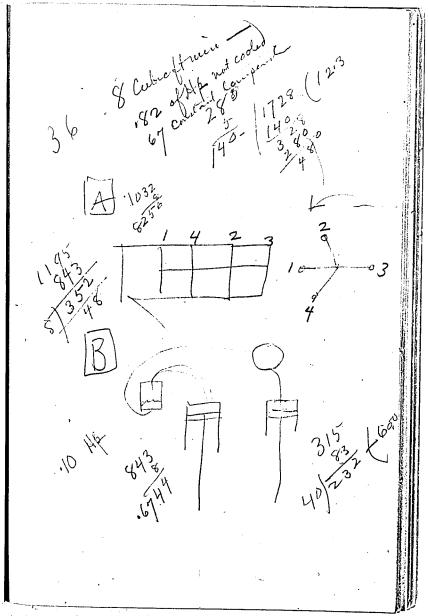
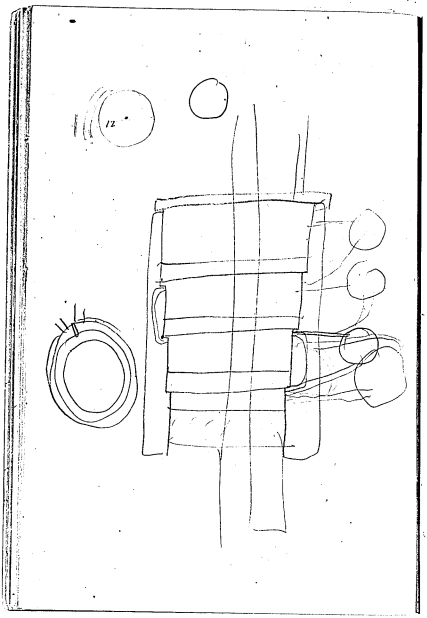
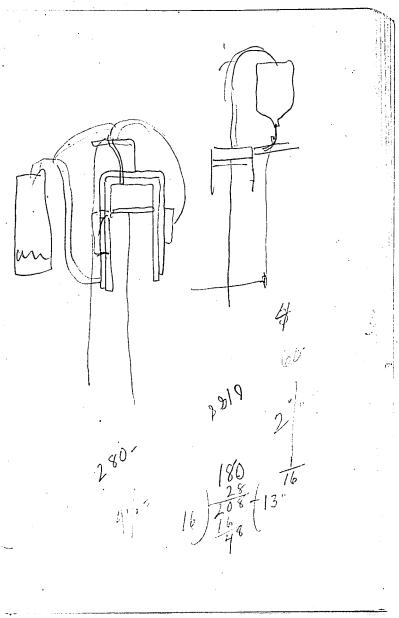
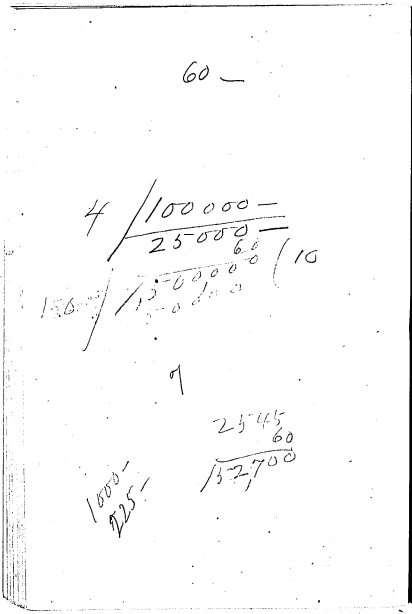

500 LBS
10
46
7




A
B
1 4 2 3
2 1 3 4


12"


4
2.819
2.80"
180
16
13"



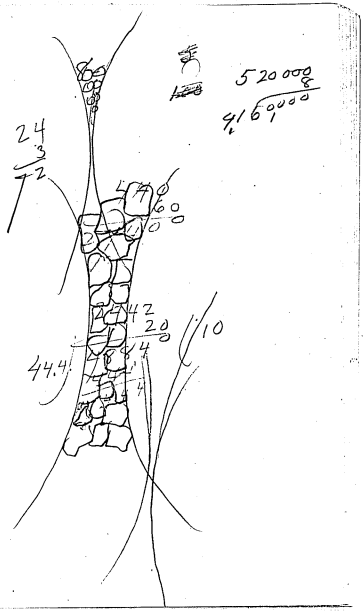
0 550 220 amperes —
1100
0 0 025 —

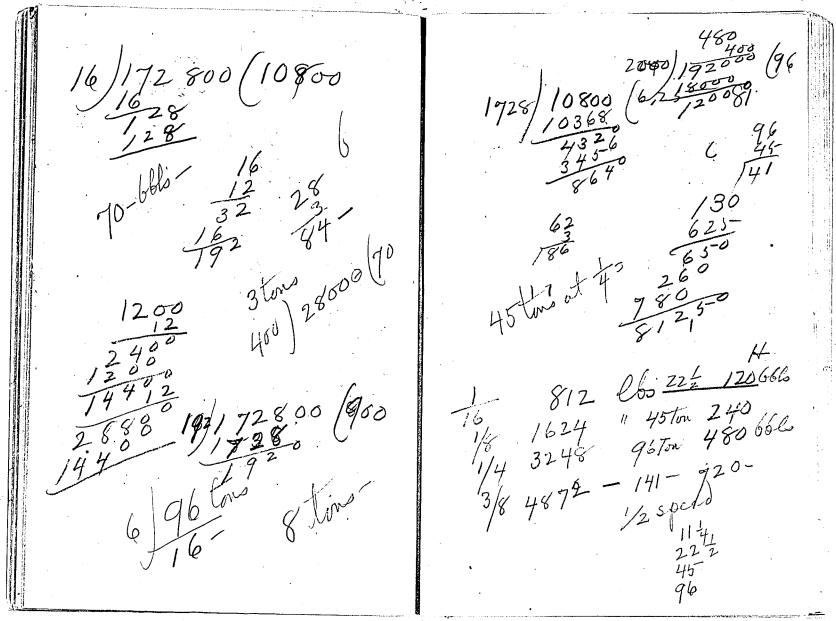
444
55
22220
22220
24442

25) 1000 (4
444
11
55
100
5
25
125 —

550 Mil amp
on 97/100 of ohm
or 24.42 ft lbs —

loss 2 1/2 per cent —
20 cells 11 amperes —
2 1/2 1/1000 of ohms ~





12 ft dia - 1 ft thick

6 Hp

144 80 1152

1200 160 1200 1200 1200

50% 1/1000 mesh

15 — 500 mesh 1:900,000 2/1000 8
15 200 124,000 5/1000 125
15 100 10,000 10/1000 1000
5 80 12/1000 1728

52 million —

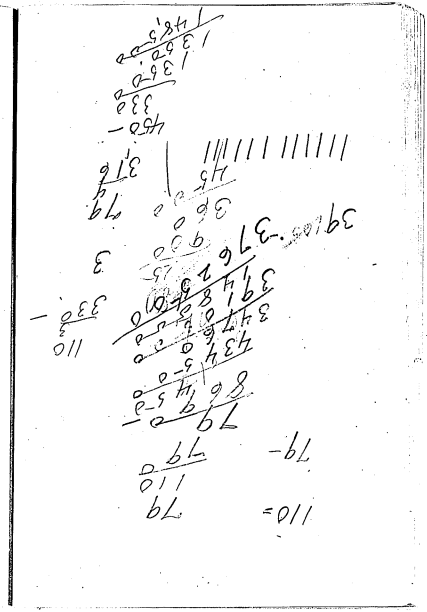
all +1000 / 100 million —
50% — 50 "

120,000

8/15
1.9

144
2
288
2
1448
17
17

125/15-000 sq mm
12.5-0
2 5 0
2 5



60 60

120

79
5000
5

79
2 | 395
1675
24
6700
3350
1020

418
60
2508 | 12/5
2000
508
500
8
40
10

1/32

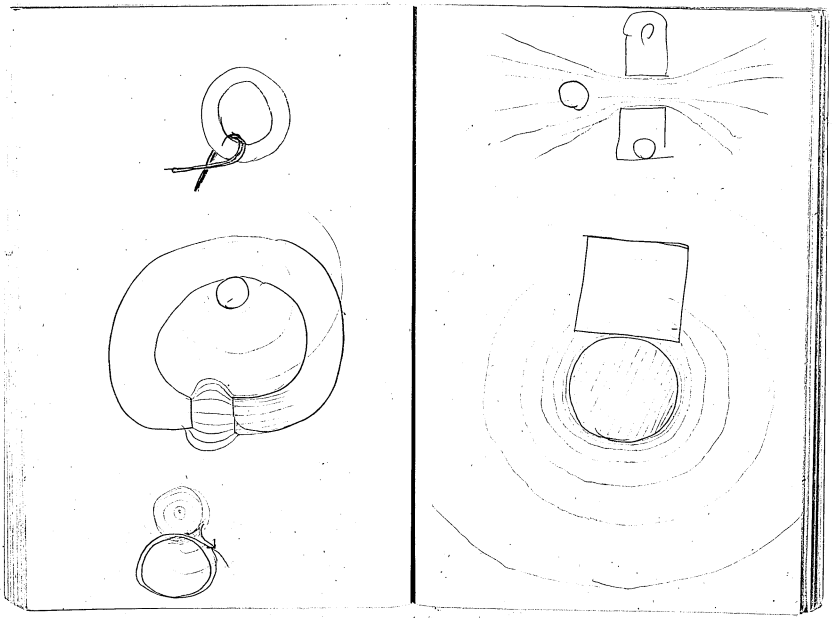
114 1/8

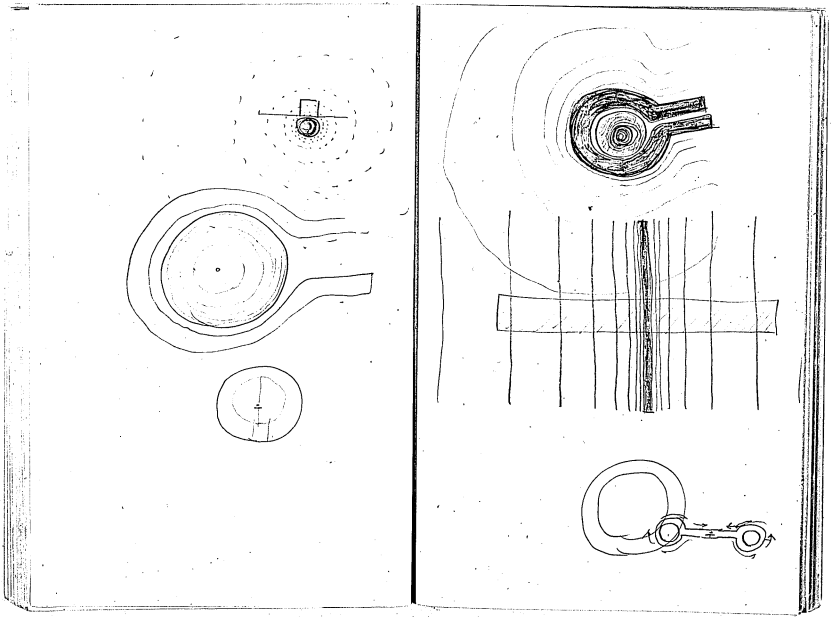
3762500 | 33000
330000
46250
33000
13250

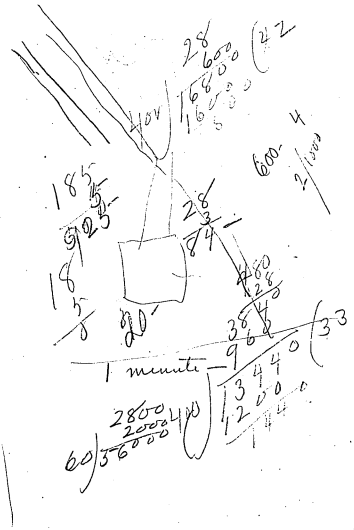
135
31
135
1200 405
4183

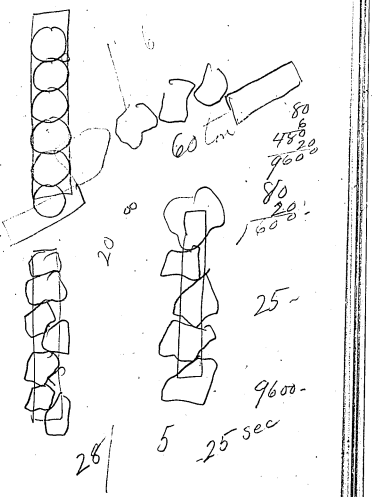
32
1/2
64
32
384

384 | 1200 | 3.1
1152
48





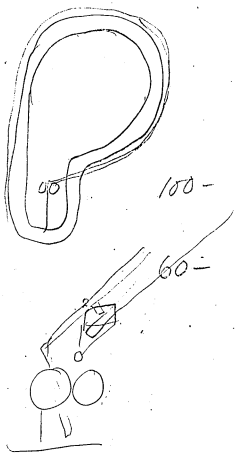

1 minute

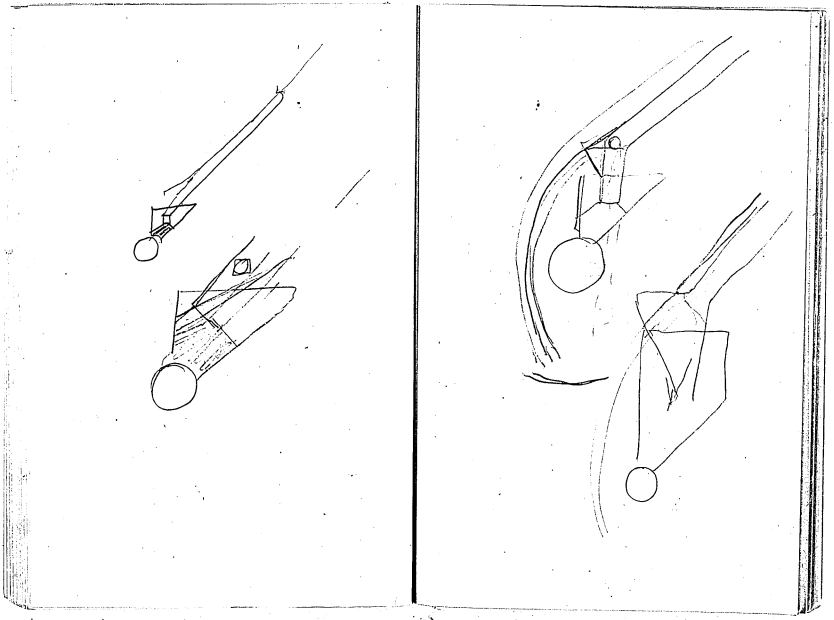

60 km
25 sec

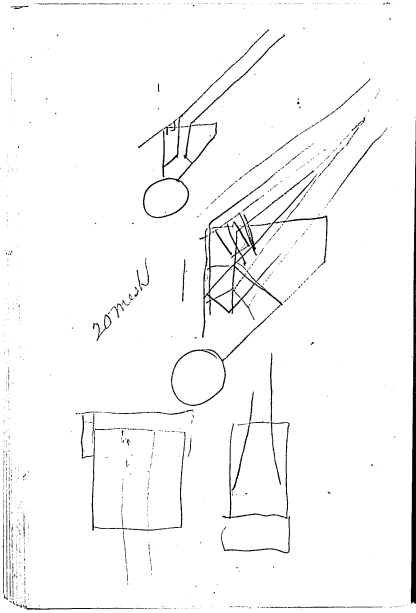
2800 lbs

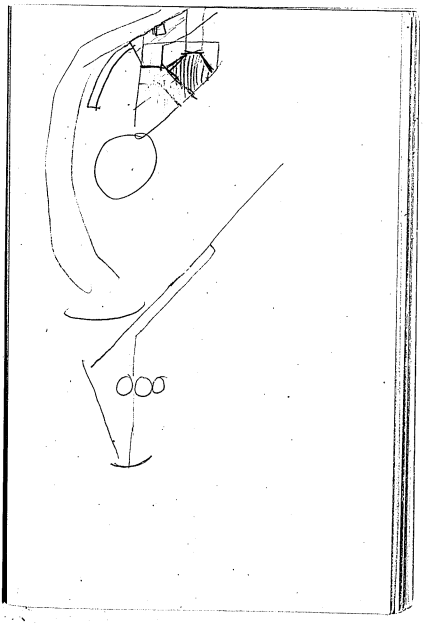
28
3
84
2000
168
1200
480
440

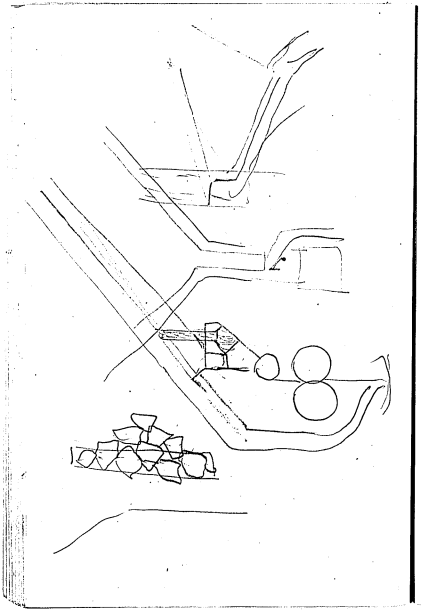
60) 2800

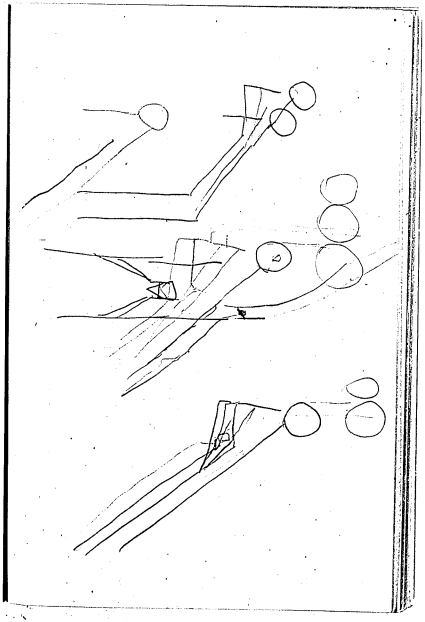


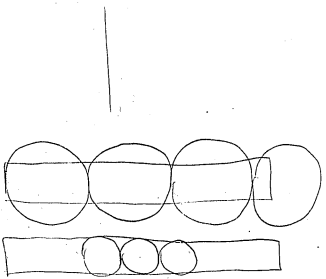


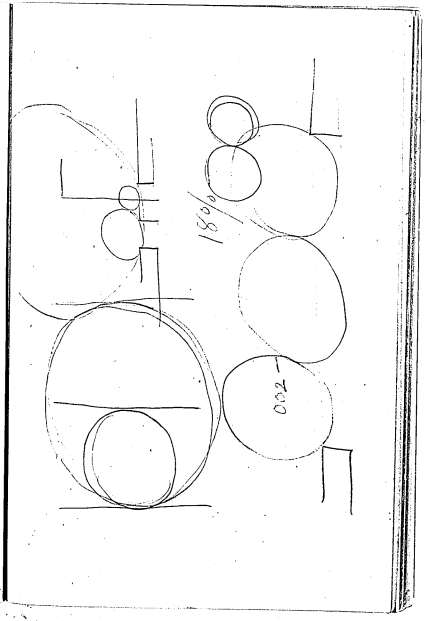

20mW

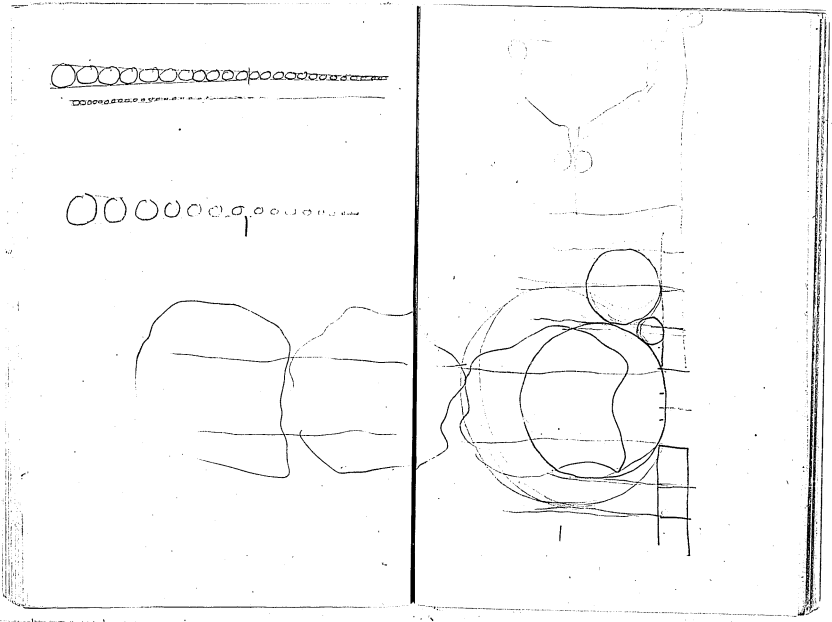


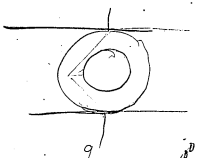


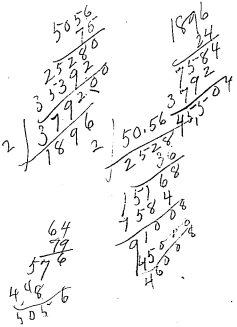


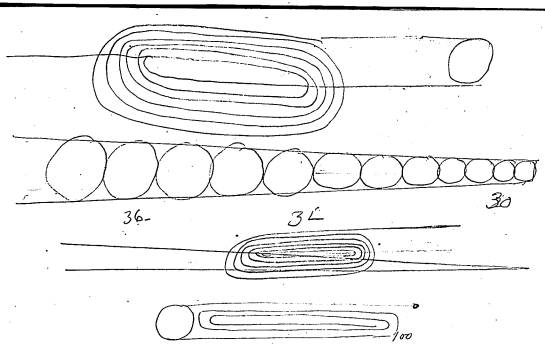


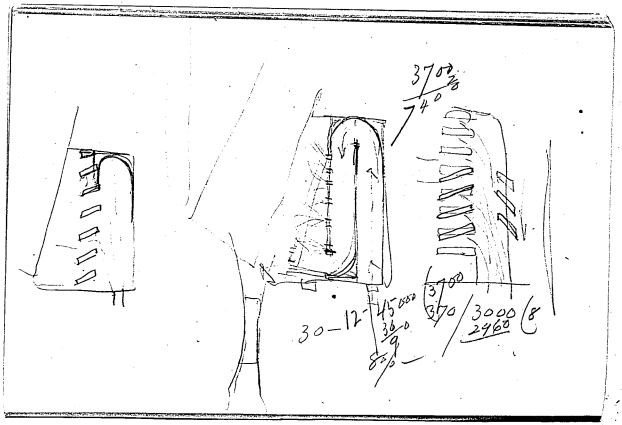

18%
002

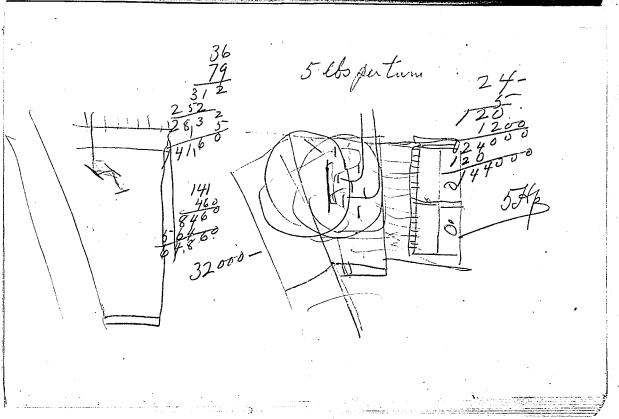


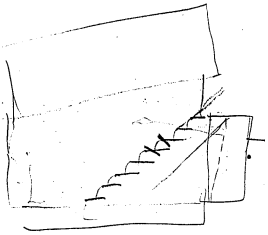


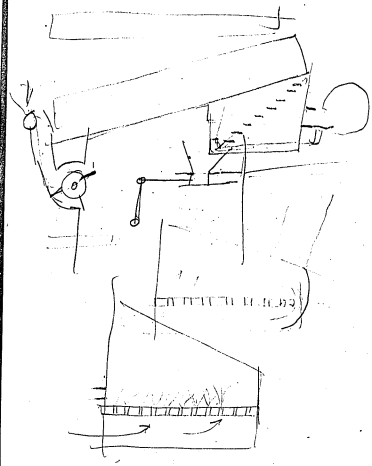


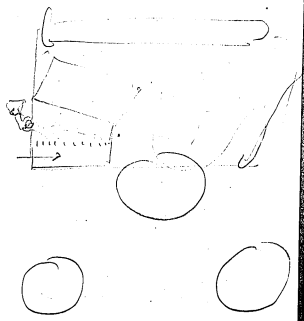

36-
3L
30
100


370
74
30–12
145000
3800
370
3000
2960
6


36
79
312
2 52
2 8 3 2
4116
141
46
846
32000
5 lbs per turn
24
5
120
1200
12400
12600
144000
5 HP







CuO Zn

KO+IK solution

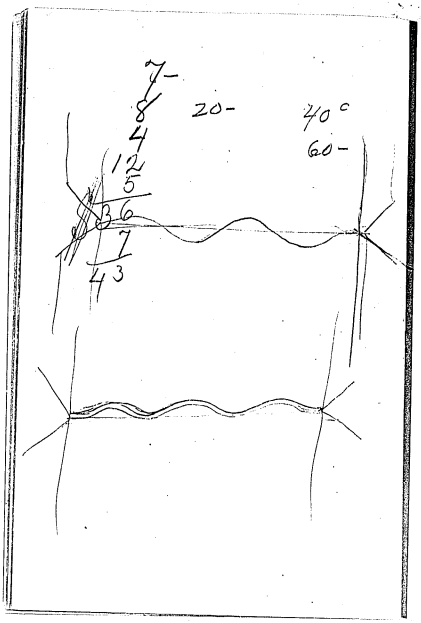
Strange When Cuprous salt

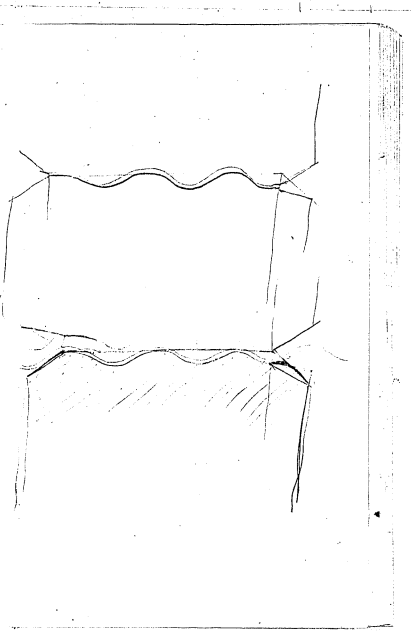
boiling add drop by drop Reddish

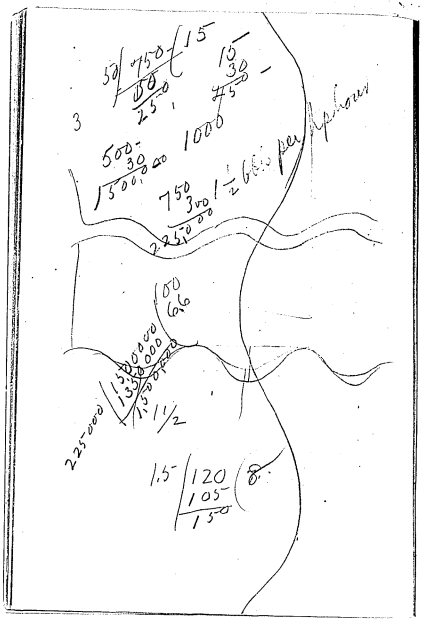
ambitious black Cu ppt

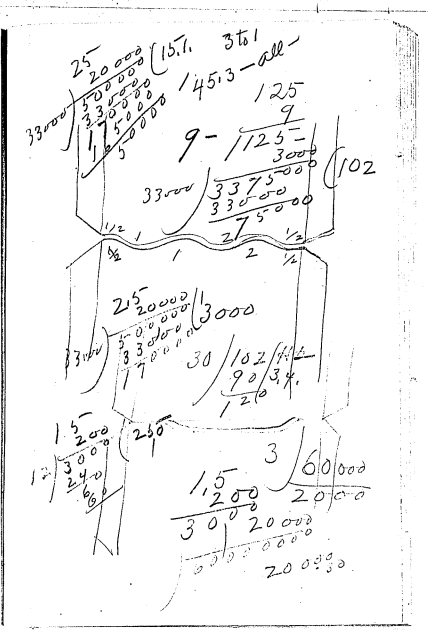
Try KCy - Changes

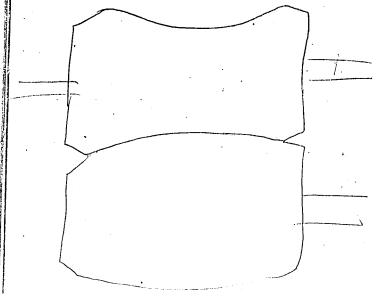
CuO not attacked

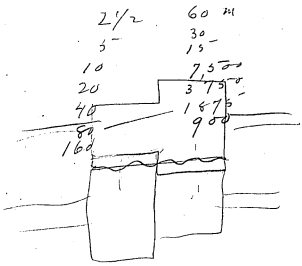

7-
8
4
12
5
36
7
43
20-
40°
60-

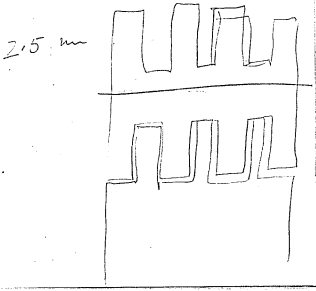


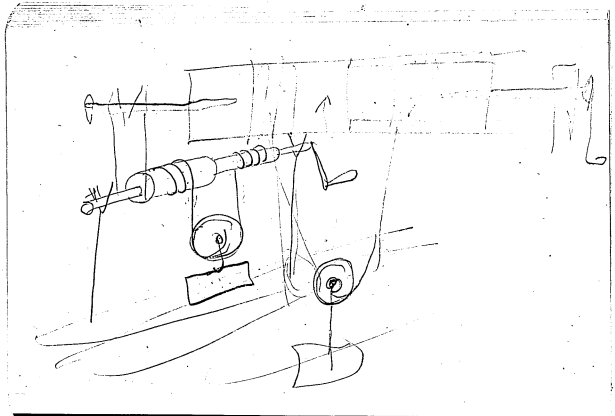

1000
1½ bbls per Spleen
225-000
1.5-
120
105-
15-
3

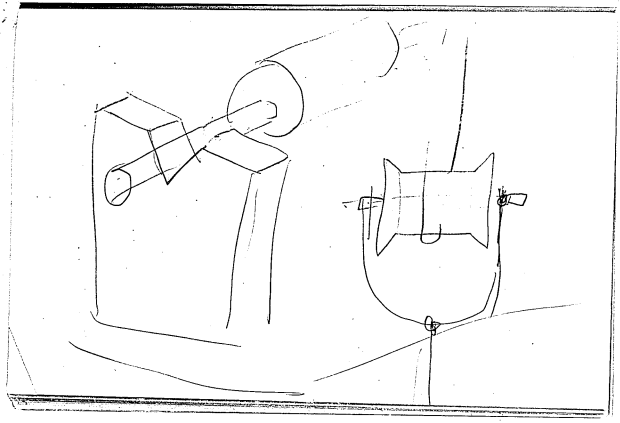

145.3 - all -
125
9-
102
33000
1½
2
250
3
60000
20000

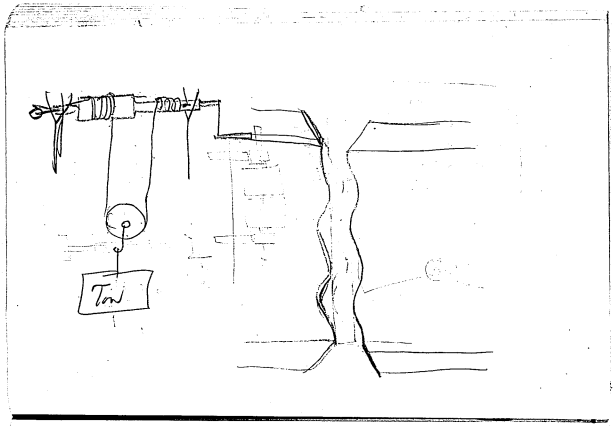


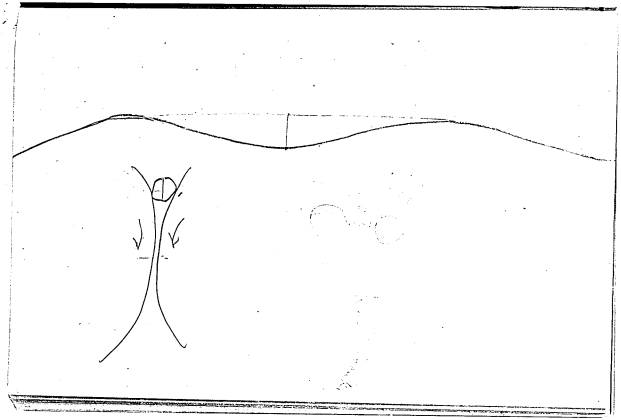

2½
5
10
20
40
80
160
60 m
30
15
7,5
3,75
1,875
0,9

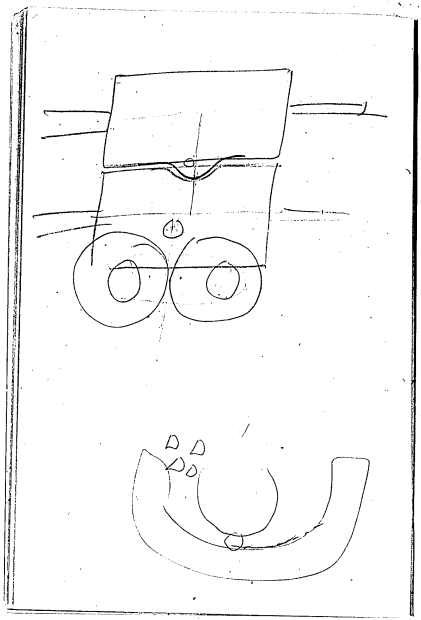

2,5 m

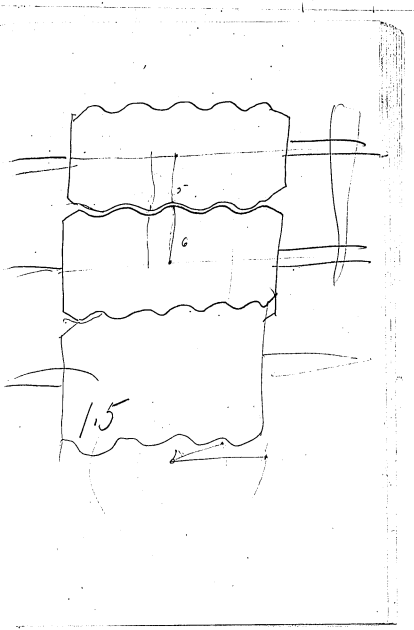


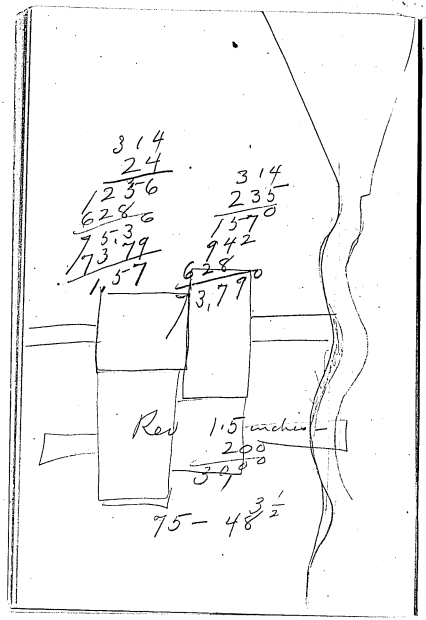


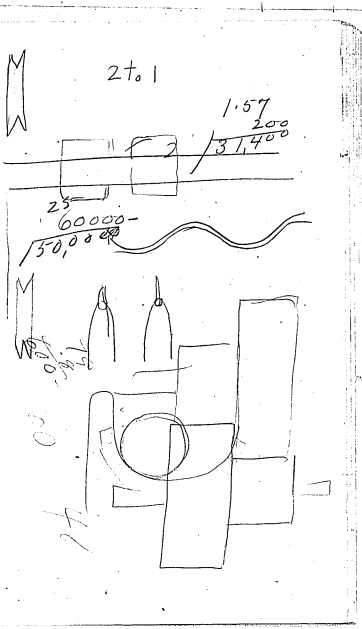

Tan






1,5


314
24
1256
6286
7536
7379
1,57
314
235
1570
942
628
3,79
Rev 1.5 inches
200
75 - 48 3/2


2 to 1
1.57
200
31,400
25
600000
30,000

48-00
17 76
65 76-
18 72
84 1 8

18720 (22
16596
2124
246
624

624
4
1872
2496

22%=

6

65
60-
3-
40,000-
2
4000

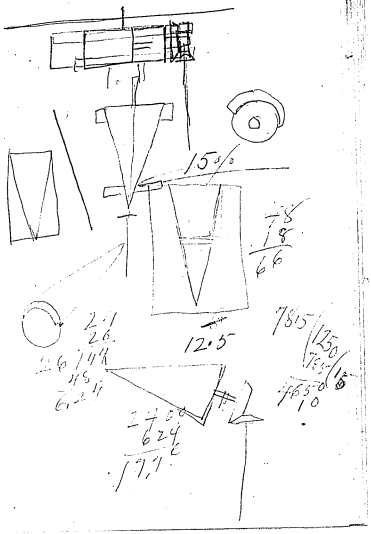
6576
2496
907²

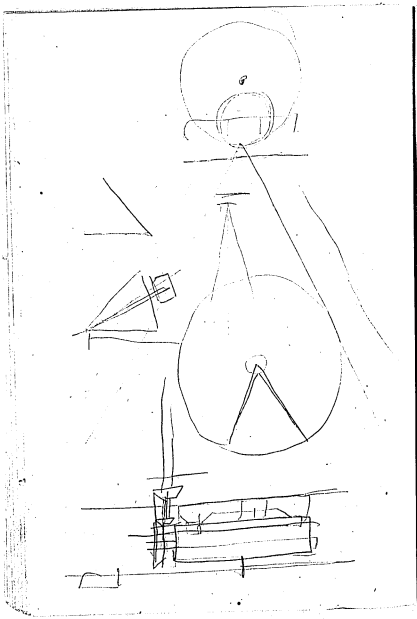
27460 (27.5
18147
68164
63504
46560

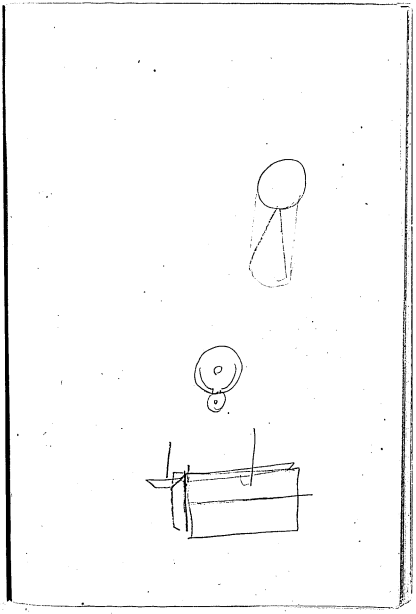
36000-

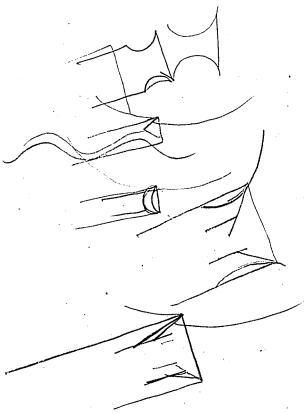
17
400
6800

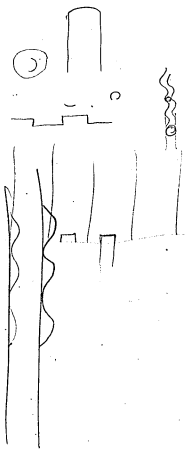
2.75
30,000-
32000-

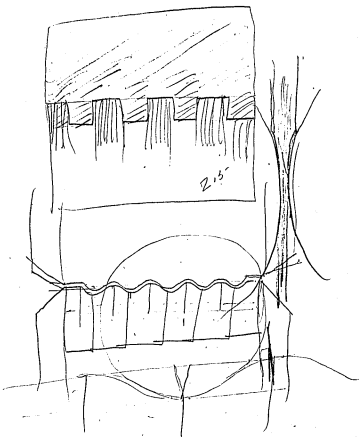

15 1/2
12.5











160 - 36 = 124

80 - 24 = 56

4

12 | 600 (50
60

1200.
60000

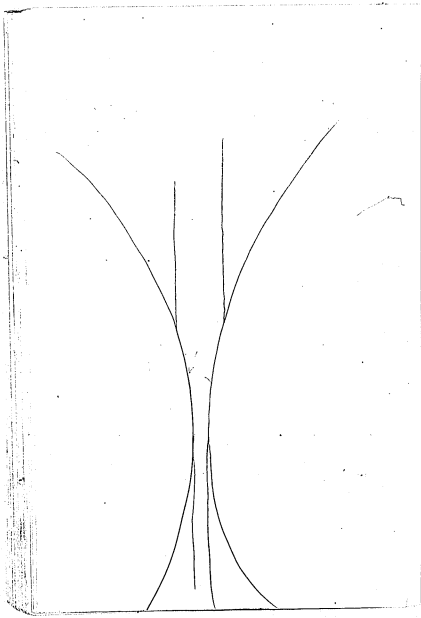
37 | 2180
726 Hp

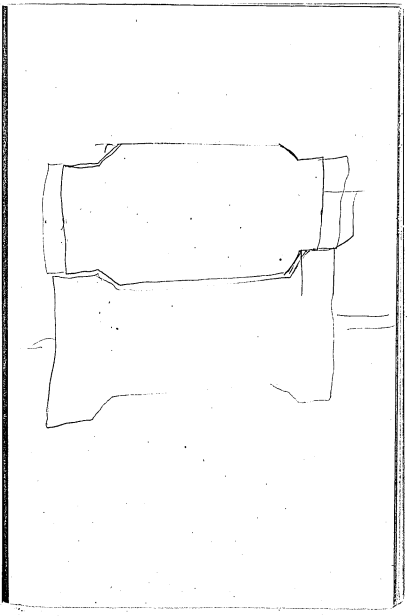
Tri Ca Phos
Mac Calsi.

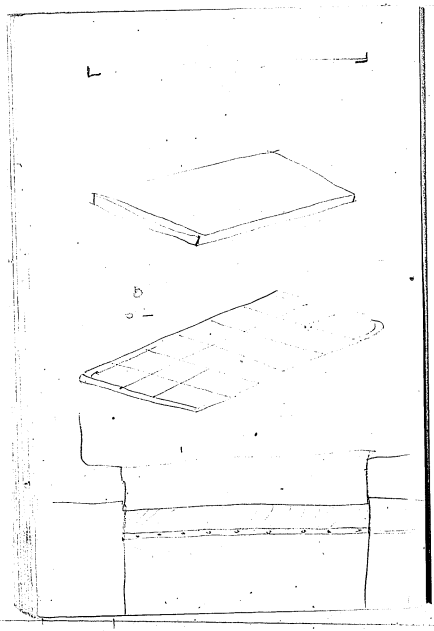
1200 ft = 726
600 " 363
300 " 182
150 " 91
75 " 46
37 " 37 | 230 (6.21
222
8.0
7.4
60

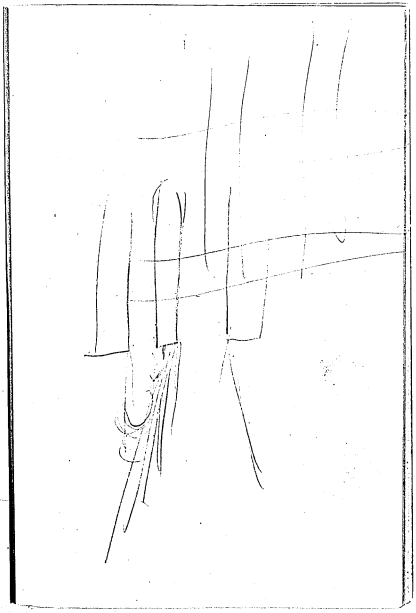
621
25
3 | 75
15
75

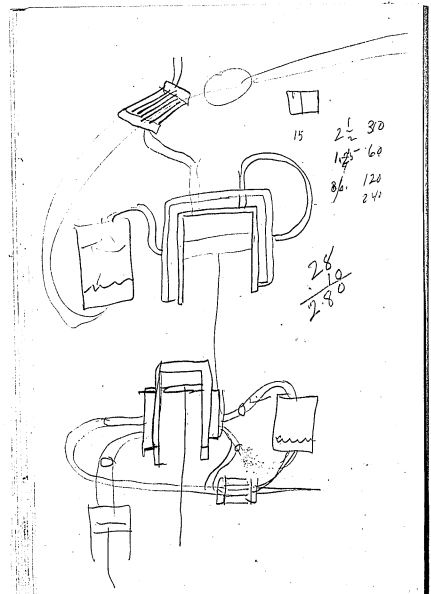
432 | 160000 (370
1296
3014
3022
1600





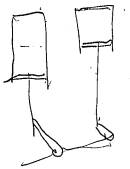






15 2½ 30
1⅞ 60
8⅛ 120
240

28 · 10 / 280



160 / 1728 (10.8
160
1280
1280

62
25
310
124
155

28
62
56
168
6

18 / 173
12
36
18
216

108
28
2 / 36
10 / 6.8

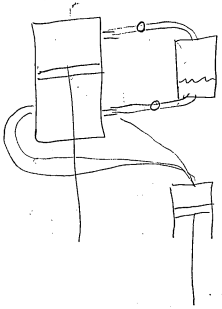
10.5 Cubic
84
84

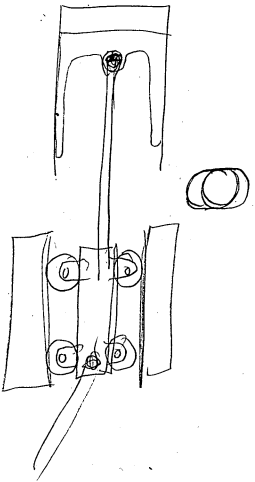
6.5
40
40
1 3 27 21

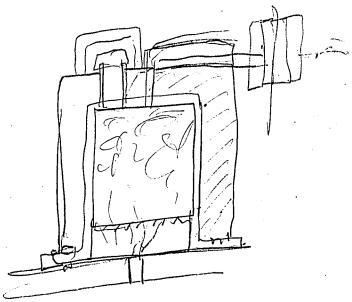
1/4 -

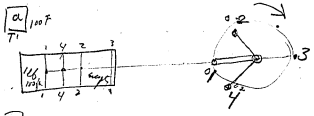
4 / 300
75 inches

36 36 / 290 (1/8
288 288
36 -



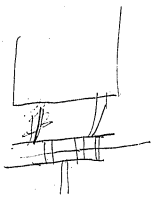


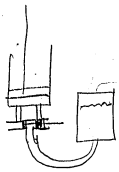


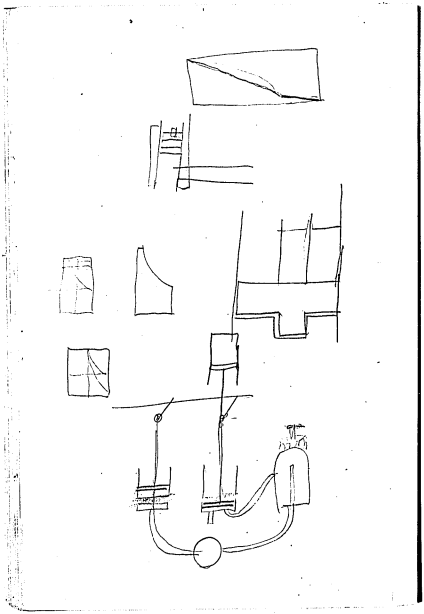


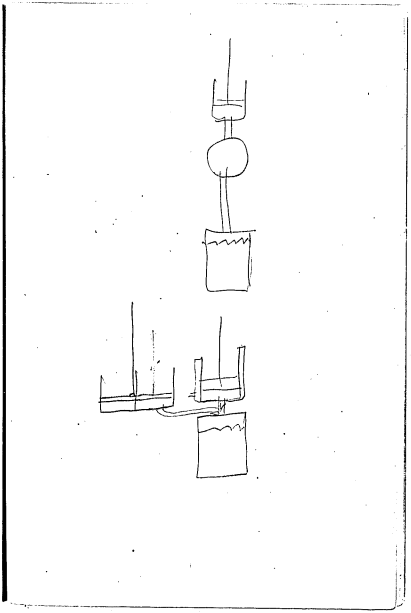
β T_3

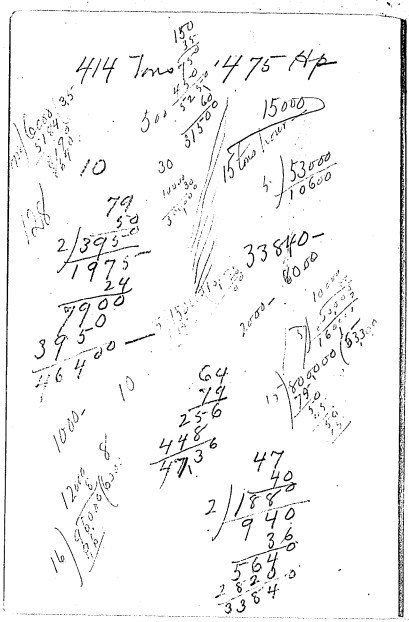
11 position pres Vol + Temp Equals 1

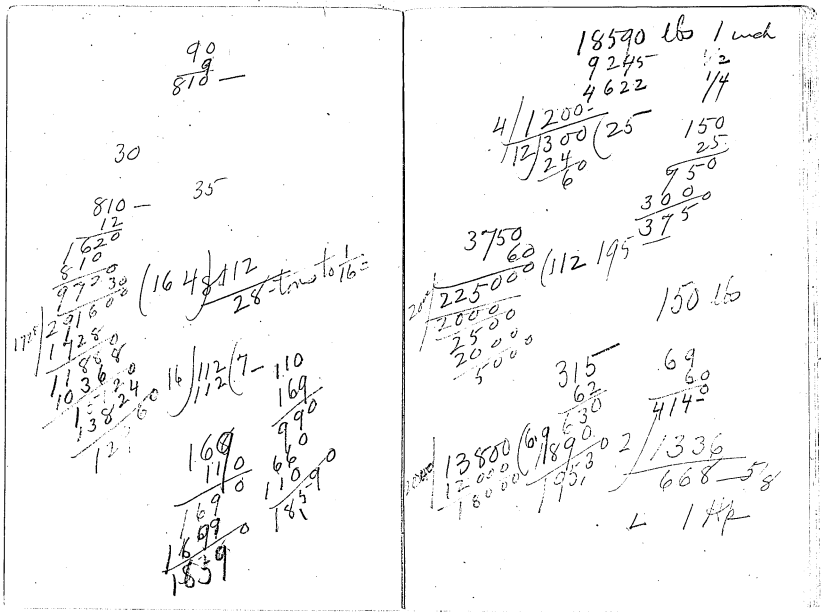


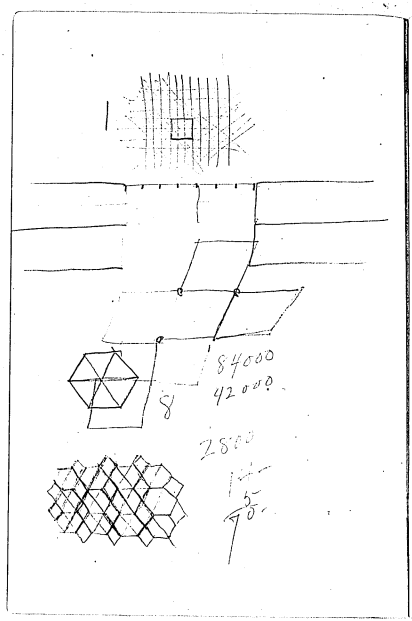




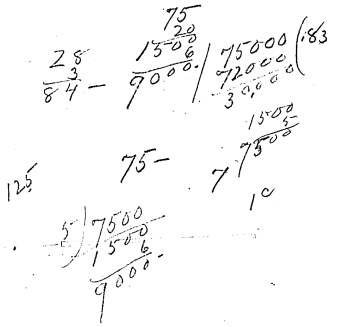


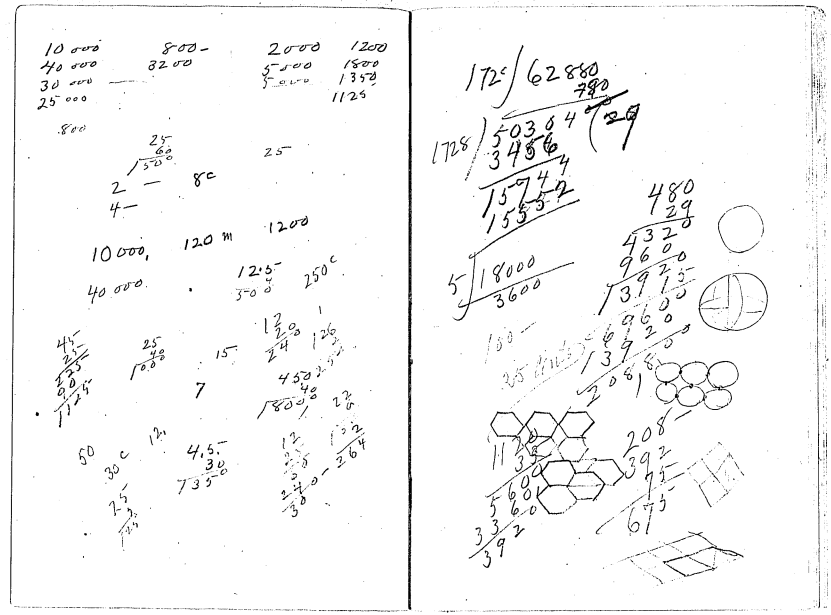

414 Tons
475 Hp
15000
53000
10600
338400
60000
64
74
256
44836
47
40
1880
940
360
564
282
33840
1975
3950
7900
24
79
10
30
1000
1300
266,666
3,333,000
20000
60
300




84000
42000
2800

$75 pair -





5240 (1310
80 | 104890
80
240
240
80
80

1310 ft

1 ft — 80 ft — 4/4 needle
2 160

600 ft —

1100 - 6" 1 ft 1½ deg
2 6
4 — 24 —

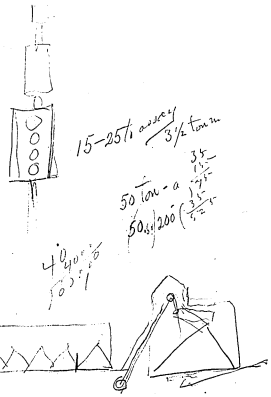
5240 · 137 / 1370 / 685 / 1048 / 5240 / 137 | 208800 (15
1370
7150
6850
1370 ft needed
5240 deg
6 — 40
1½ — 80

20 ft 1 ft-ring

62480 62500
5240
48 · 2620 / 5 / 24 / 100 / 96 / 40 / 36 / 4
250000 (2083 3

137 | 260000 (1170
1370
2370
1370
9390
9590

4.4 to
5240
1200
1048
5240
2650


15–25 ton assort
3½ ton
50 ton - a
50 x 200

Heat- Sledge coil Syste 3000
for Elevator 4500
Big Load - 3600
25 Horses - 4000
50 Smaller 12000
Terminals Motor Starters - 800
Carried 22855
50705

75000

1600
2850
12850
2000
3
47481

68
7
476
60
416

20

400-

12 Heavy rail shafts 2200
Taking out shafts - 200
Grooving shafts - 80
New outlet casings - 25
Fixing brasses - 200
Assembling rails

New plates 1st 36 - 150
Fixing Cranes - 400
New take wheels
Screens - 1200
Shafts -
445 Batts - 4000
Roller recessing 844 - 2000
Change Chute -
Seperators 2 stock ht - 6000
17 Mixers - 1560
Ore dock blowing 2000
Sand House 1500
Shaker Bags 1 - 500
Bldg. at 3 Ht 2 800
22853

9084 - 180
1 12
18078 360
180
216

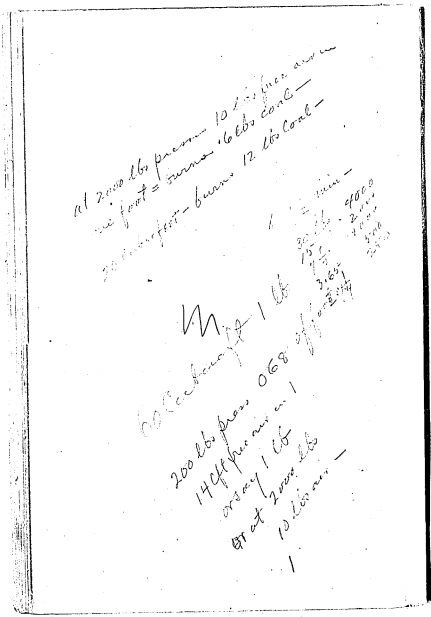
Jury

144
460
1320
880
1912
10812
9037

36
36
216
108
1296
10361,6

1036
36
6216
3108
37296
34560
2736
17280
10080

(21,6

173 4) 4140 (23 5 1728)
3468
6720
3202

235
460
1410
940
108100